

# Enhanced Removal of $\text{Cu}^{2+}$ and $\text{Pb}^{2+}$ Ions from Wastewater via a Hybrid Capacitive Deionization Platform with $\text{MnO}_2/\text{N}$ -Doped Mesoporous Carbon Nanocomposite Electrodes

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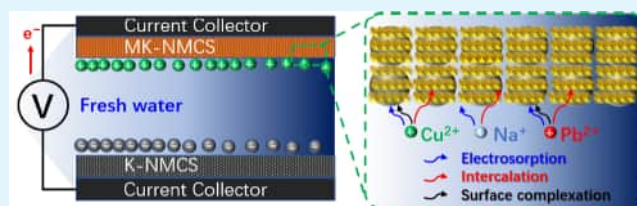
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Supporting Information

**ABSTRACT:** Integrating  $\text{MnO}_2$  with carbon is a reliable strategy to improve capacitive deionization (CDI) performance by leveraging the unique properties of both components (i.e.,  $\text{MnO}_2$  and carbon). However, the influences of preliminary functionalization of carbon (e.g., nitrogen doping, KOH activation) and pairing of cathodes and anodes on the CDI performance have yet to be systematically explored. Herein, we prepared a group of  $\text{MnO}_2$ -decorated mesoporous carbon composites with nitrogen as a dopant (i.e., MK-NMCS, K-NMCS, NMCS, and CS), and systematically evaluated the desalination performance of various cathode//anode pairs in a hybrid capacitive deionization (HCDI) for capturing  $\text{Na}^+$ ,  $\text{Cu}^{2+}$ , and  $\text{Pb}^{2+}$ , respectively. Of all electrodes, the MK-NMCS//K-NMCS pair demonstrates the optimum desalination performance based on salt adsorption capacity (SAC) and cycling stability, offering a SAC of  $25.4 \text{ mg g}^{-1}$  and a SAC retention of 102.4% after 50 consecutive charge–discharge cycles at 1.2 V in 500 ppm of NaCl solution. In addition, the MK-NMCS//K-NMCS electrodes also show the maximum ion adsorption capacity (IAC) toward  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  ions compared to other cathode//anode pairs, attaining an IAC of 37.0 and 30.0  $\text{mg Cu}^{2+}$  per gram electrode materials at 1.2 V in 500 and 200 ppm of  $\text{Cu}^{2+}$  solutions, respectively (cf. 32.2  $\text{mg of Pb}^{2+}$  per gram of electrode materials in 200 ppm of  $\text{Pb}^{2+}$  solution). Besides, these electrodes exhibit excellent cycling stability when applied in removing each heavy metal ion separately, with IAC retentions of 90.0 and 98.5% after 50 cycles toward  $\text{Cu}^{2+}$  and  $\text{Pb}^{2+}$  ions, respectively. Mechanical analysis reveals that both heavy metals are likely to be sequestered via capacitive electrosorption by carbon, intercalation with  $\text{MnO}_2$ , and surface complexation at the external surface of the  $[\text{MnO}_6]$  octahedral layers. Our results demonstrated a great potential of the  $\text{MnO}_2$ -decorated N-doped carbon//prefunctionalized carbon pairs, in particular, the MK-NMCS//K-NMCS electrode pair for capturing heavy metal ions via HCDI platforms. Such prefunctionalization and pairing strategies are very promising for screening high-performance composite electrodes for wastewater remediation.

**KEYWORDS:** copper, lead, hybrid capacitive deionization (HCDI), birnessite, intercalation



## 1. INTRODUCTION

The global water shortage, deteriorated by climate change and water pollution, has become a critical concern impacting many regions worldwide.<sup>1–3</sup> Climate change contributes to this crisis by altering precipitation patterns, resulting in more frequent and severe droughts, and disrupting the natural water cycle.<sup>4</sup> Concurrently, water pollution further exacerbates the scarcity of freshwater.<sup>5</sup> Among the various pollutants, heavy metals pose a significant threat to water bodies. Rivers, for example, which are vital sources of freshwater, are particularly vulnerable.<sup>6</sup> When contaminated by heavy metals, such as copper ( $\text{Cu}^{2+}$ ) and lead ( $\text{Pb}^{2+}$ ), these rivers will inevitably experience severe ecological damage.<sup>6,7</sup> Heavy metals are toxic to macroscopic organisms, leading to their rapid death. This, in turn, impacts microorganisms essential for the river's self-purification processes, ultimately diminishing the river's ability to recover its health over time.<sup>8</sup> The contamination of rivers with heavy metals has profound consequences for both the environment and human health. Copper and lead ions, for

example, are notorious for their harmful effects. Copper, when present in high concentrations, can disrupt aquatic ecosystems, causing detrimental effects on fish and plant life, while also posing risks to human health, such as gastrointestinal distress and liver damage.<sup>9</sup> Lead ions are even more dangerous; they can accumulate in the food chain, leading to severe neurological and developmental issues, particularly in children.<sup>10</sup> The persistence of these metals in the environment further complicates this issue, making remediation efforts crucial.

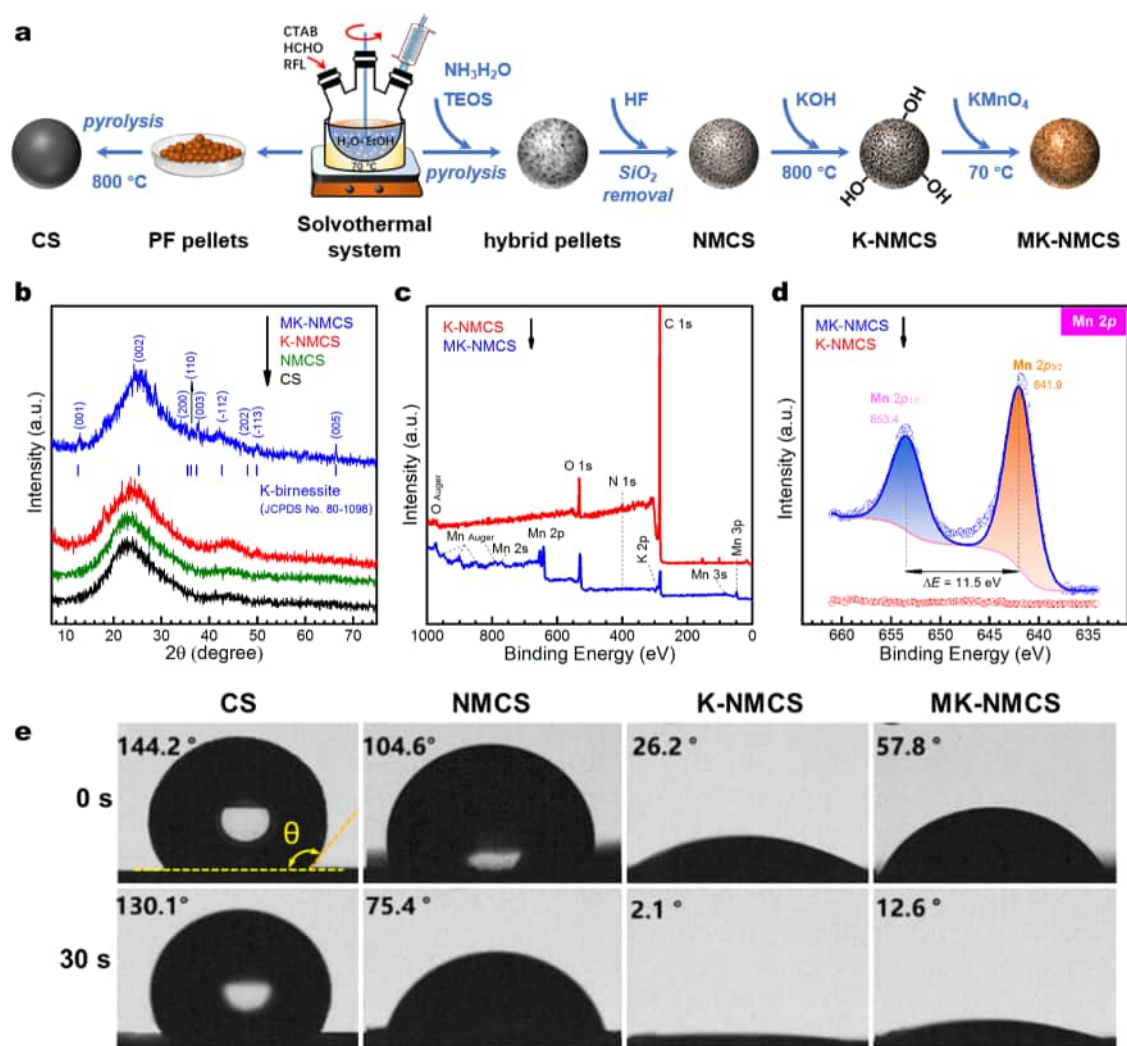
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**Figure 1.** (a) Schematic illustration of the preparation of  $\text{MnO}_2$  anchored mesoporous carbon nanocomposites; (b) X-ray diffraction (XRD) patterns; (c) survey X-ray photoelectron spectroscopy (XPS) spectra; (d) Mn 2p XPS region of K-NMCS and MK-NMCS (note:  $\Delta E$  of the two split components of the Mn 2p peak is about 11.5 eV, indicative of the  $\text{MnO}_2$ ); and (e) water contact angle ( $\theta$ ) evolution of these  $\text{MnO}_2/\text{MCS}$  nanocomposites after contacting with water from the beginning (0 s) to 30 s (30 s).

Tackling heavy metal contamination involves various strategies for wastewater decontamination and water purification.<sup>11</sup> Traditional methods include chemical precipitation, filtration, and ion exchange, but these approaches can be costly and less efficient.<sup>12</sup> Among the cutting-edge technologies, capacitive deionization (CDI) has emerged as a promising method for heavy metal ion removal.<sup>13–16</sup> CDI utilizes an electric field to drive ions from water into porous electrodes, effectively removing contaminants.<sup>17–19</sup> This technology offers several advantages, such as high efficiency, lower energy consumption, and the potential for regeneration of the electrodes, making it a viable solution for mitigating heavy metal pollution and addressing water scarcity challenges.<sup>20–22</sup> So far, a large variety of electrode materials have been extensively used in CDI for capturing heavy metals from water, which can be broadly categorized into nonFaradaic (e.g., carbon-based matter) and Faradaic (charge transfer) materials.<sup>23,24</sup> Among various Faradaic (charge transfer) materials, manganese dioxide ( $\text{MnO}_2$ ) has emerged as a promising electrode material for CDI due to its low cost, high stability, and high theoretical specific capacitance of  $1370 \text{ F g}^{-1}$ .<sup>25–27</sup> However, like most common transition metal oxides,  $\text{MnO}_2$

has a poor electrical conductivity, which limits its CDI performance, such as salt adsorption rate (SAR) and salt adsorption capacity (SAC).<sup>28–30</sup>

To this end, integrating  $\text{MnO}_2$  with carbon-based materials of high conductivity appears to be a promising strategy.<sup>31</sup> Since  $\text{MnO}_2$  has high pseudocapacitance that contributes to high charge storage capacity and rapid charge/discharge kinetics, carbon-based materials, such as activated carbon or graphene, provide high surface area and electrical conductivity. The combination of  $\text{MnO}_2$  and carbon materials can leverage the unique electrochemical properties of both components, yielding manganese dioxide/carbon ( $\text{MnO}_2/\text{C}$ ) composite electrodes with superior CDI performance.<sup>32–36</sup> Early studies on  $\text{MnO}_2/\text{C}$  composite electrodes in CDI have demonstrated their effectiveness in both ion removal and heavy metal ion capture. For instance, El-Deen and colleagues reported a graphene-wrapped  $\text{MnO}_2$  electrode ( $\text{MnO}_2$ -nanorods@graphene), which demonstrated distinct SAC ( $5.01 \text{ mg g}^{-1}$ ), high salt removal efficiency ( $\sim 93\%$ ), and good recyclability.<sup>32</sup> Chen et al. revealed that composting  $\text{MnO}_2$  with multiwalled carbon nanotubes (MWCNTs) can enhance the SAC of the virginal  $\text{MnO}_2$  electrode by 4.1 times, and the  $\text{MnO}_2/$

MWCNTs composite electrode also showed excellent recyclability and rapid regeneration process.<sup>33</sup> Using an electrodeposition technique, Liu et al. showed that the electrodeposited MnO<sub>2</sub>/AC composite electrode presents a superior SAC (9.3 mg g<sup>-1</sup>) due to the combination of capacitive and Faradaic process.<sup>34</sup> To achieve a better CDI performance of a pristine ordered mesoporous carbon (OMC), Zhao and co-workers decorated OMC with manganese oxide nanoparticles by an impregnation method and showed that the enhanced electrosorption performances were attributed to the Faradaic interfacial process between the guest MnO<sub>2</sub> nanoparticles and the OMC matrix.<sup>35</sup> Besides, it is also shown that graphene-coated single-walled carbon nanotube (SWCNT) aerogels decorated with MnO<sub>2</sub> can be used as freestanding electrodes for superelastic pseudocapacitors, which is also promising for CDI application.<sup>36</sup> Similarly, it has been well-documented in recent reports that integrating MnO<sub>2</sub> with carbon can efficiently improve the CDI performance toward Cu<sup>2+</sup> and Pb<sup>2+</sup> ions.<sup>37–40</sup> Birnessite ( $\delta$ -MnO<sub>2</sub>), for example, has been shown as a promising electrode candidate for capacitive capturing Cu<sup>2+</sup> from water.<sup>37,38</sup> By electrodepositing MnO<sub>2</sub> and polypyrrole (PPy) on the surface of graphene oxide (GO), Zhang et al. prepared a GO/PPy/MnO<sub>2</sub> composite electrode that displays an excellent SAC toward Cu<sup>2+</sup> ion (38.4 mg g<sup>-1</sup>).<sup>39</sup> Likewise, Liu and colleagues developed a three-dimensional (3D) graphene/MnO<sub>2</sub> nanocomposite (PGA/MnO<sub>2</sub>) electrode that shows high SACs toward various metal ions (e.g., Pb<sup>2+</sup>, Cu<sup>2+</sup>, and UO<sub>2</sub><sup>2+</sup>) due to the 3D porous nanostructure as well as the synergetic action between MnO<sub>2</sub> and graphene.<sup>40</sup> It is well-documented that both nitrogen (N) doping and KOH activation can significantly enhance the specific surface area, wettability, and specific capacitance of carbon-based electrodes, and thereof their CDI performance.<sup>41–43</sup> More recently, it has been shown that N-doping of carbon with nonmetallic elements can greatly improve its affinity toward many metal ions including Pb<sup>2+</sup> and Cu<sup>2+</sup> ions.<sup>44,45</sup> However, the interactions between such ions and the MnO<sub>2</sub>-decorated carbon doped with nitrogen at CDI platforms have not been explored so far.

Inspired by the aforementioned studies and aimed at elaborating the potentials of MnO<sub>2</sub>-decorated N-doped mesoporous carbon electrodes in the capacitive removal of heavy metals, we prepared a set of MnO<sub>2</sub>-decorated mesoporous carbon spheres (MnO<sub>2</sub>/MCS) and investigated the capacitive removal performance of these MnO<sub>2</sub>/MCS electrodes for both Cu<sup>2+</sup> and Pb<sup>2+</sup> ions from wastewater at CDI platforms systematically. We elucidated insights into the improvement of the capacitive removal of Cu<sup>2+</sup> and Pb<sup>2+</sup> ions over these electrodes via microstructural characterization, electrochemical analysis, and electrochemical desalination experiments. Meanwhile, we evaluated the impacts of cell voltage and salt concentration of the feed solution on the desalination performance, respectively. We also examined the cycling stability of the MnO<sub>2</sub>/MCS electrodes and the possible mechanisms of Cu<sup>2+</sup>/Pb<sup>2+</sup> uptake. Overall, this work underscores the potential of MnO<sub>2</sub>/MCS nanocomposites in addressing both general desalination and specific heavy metal ion removal challenges.

## 2. MATERIALS AND METHODS

**2.1. Chemicals.** Cetyltrimethylammonium bromide (CTAB, 99%), potassium permanganate (KMnO<sub>4</sub>, 99.5%), potassium hydroxide (KOH, 85%), ammonium hydroxide (NH<sub>4</sub>OH, 25–

28%), resorcinol (RFL, 99%), formaldehyde (HCHO, 37–40%), tetraethyl orthosilicate (TEOS), and hydrofluoric acid (HF, 40%) were purchased from Sinopharm Chemical Co. Sodium chloride (NaCl, 99.5%), copper chloride (CuCl<sub>2</sub>, 99.99%), and lead chloride (PbCl<sub>2</sub>, 99.99%) were obtained from Aladdin Chemical Co., Ltd. All chemicals were used as received. Ultrapure deionized water (DI H<sub>2</sub>O, 18.2  $\Omega$  cm at 25 °C) was used for preparing the solutions.

**2.2. Preparation of MnO<sub>2</sub>/Mesoporous Carbon Nanocomposites.** As depicted in Figure 1a, MnO<sub>2</sub>/mesoporous carbon nanocomposites were prepared via a multistep synthesis approach. Typically, 4.0 g of CTAB, 1.1 g of RFL, and 0.2 mL of NH<sub>4</sub>OH were first dissolved in a three-neck flask containing an EtOH/water solution (80 mL/200 mL, v/v), to which 1.48 mL of HCHO and 6 mL of TEOS were then added and solvothermally treated at 70 °C for 24 h under moderate stirring conditions (60 rpm). The resulting pellets were collected by centrifugation and rinsed several times with excess DI water and EtOH, followed by drying in an oven at 80 °C overnight. The dry pellets were then pyrolyzed at 800 °C for 2 h under a N<sub>2</sub> atmosphere. After cooling down to room temperature, the synthetic hybrid pellets were further rinsed and etched with 10% HF solution to remove the silicon dioxide (SiO<sub>2</sub>) component, yielding N-doped mesoporous carbon spheres denoted as NMCS.

Activation of NMCS pellets by KOH was achieved by mixing 0.5 g of such pellets in 20 mL of KOH solution (100 g L<sup>-1</sup>) at 80 °C overnight. The obtained dry sample was sequentially pyrolyzed at 800 °C under a N<sub>2</sub> atmosphere, followed by cooling, rinsing with 10% HCl (for removal of residual K<sup>+</sup>) and excess water, and drying at 80 °C overnight. The synthetic pellets are denoted by K-NMCS. Further, anchoring manganese oxide onto the above K-NMCS was carried out by hydrothermally mixing 0.2 g of K-NMCS with 50 mL of KMnO<sub>4</sub> solution (0.05 M) at 70 °C for 24 h, followed by rinsing with excess water and drying at 80 °C overnight. The MnO<sub>2</sub>-loaded sample was denoted by MK-NMCS. For comparison, the pure mesoporous carbon spheres (denoted by CS) were also prepared using the same protocol as that of NMCS without the addition of NH<sub>4</sub>OH and TEOS (i.e., the direct pyrolysis route). All synthetic pellets are stored in a glass desiccator before use.

**2.3. Materials Characterization and Electrochemical Measurements.** X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), scanning electron microscopy (SEM), energy-dispersive X-ray (EDX) spectroscopy, contact angle analysis, and N<sub>2</sub> absorption–desorption measurement were applied to characterize the as-prepared MnO<sub>2</sub>/mesoporous carbon nanocomposites. More details about the characterizations are provided in Text S1 (Supporting Information). Electrochemical measurements, including cyclic voltammetry (CV), galvanostatic charge–discharge (GCD), and electrochemical impedance spectroscopy (EIS) were performed in 1.0 M NaCl solution on a CS310H electrochemical workstation (Correst Inc., China). The measurements were conducted with a three-electrode system containing a 1 cm  $\times$  2 cm graphite paper precoated with the MnO<sub>2</sub>/mesoporous carbon nanocomposites (working electrode), a platinum foil electrode (counter electrode), and an Ag/AgCl (3 M KCl) electrode (reference electrode). A detailed description of the electrochemical measurement is elaborated in Text S2 (Supporting Information).

**2.4. Capacitive Deionization Test.** The electrodes for CDI performance evaluation were prepared by using the same recipe of electrodes for electrochemical measurements (Text S2). Typically, 50 mg of active materials was mixed and ground with a desired amount of acetylene black and poly(vinylidene fluoride) (PVDF) to achieve a final mass ratio of 8:1:1, followed by dispersing in 4 mL of N,N-dimethylformamide (DMF) by sonication for 60 min to form a homogeneous slurry. The slurry was sequentially applied onto a clean graphite paper (5 cm  $\times$  5 cm), which was dried in a vacuum at 100 °C overnight before mounting onto the CDI cell (Figure S1).<sup>27</sup> The CDI tests were performed in batch mode under constant voltage conditions. Voltages of 0.6–1.2 V and feed solutions of 100–500 ppm of NaCl solutions were employed to evaluate the influences of cell voltage and feed solution on the CDI performance, respectively. The SAC of the electrode was determined by eq 1

$$\text{SAC} = \frac{(C_0 - C_e)V}{m} \quad (1)$$

where  $C_0$  and  $C_e$  represent the initial and the final concentration of the feed solution ( $\text{mg L}^{-1}$ ), respectively,  $V$  is the solution volume (mL), and  $m$  refers to the total mass of the active electrode material (g). More details on CDI tests are given in Text S3 (Supporting Information).

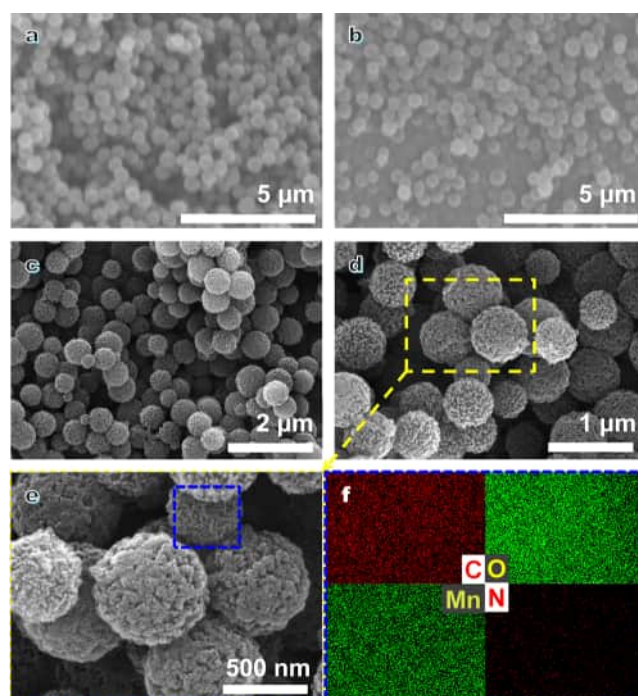
### 3. RESULTS AND DISCUSSION

#### 3.1. Physicochemical Characteristics of As-Prepared

**Materials.** The XRD patterns of the as-prepared materials are shown in Figure 1b. All of the patterns are featured by two diffuse humps in  $2\theta$  ranges of  $10\text{--}40$  and  $40\text{--}50^\circ$  irrespective of the synthetic routes, i.e., direct pyrolysis at  $800^\circ\text{C}$  (CS), doping by nitrogen (NMCS), activating with KOH (K-NMCS), and decorating with  $\text{MnO}_2$  (MK-NMCS). These diffuse humps indicate the amorphous nature of these synthetic carbon spheres.<sup>46</sup> It is noteworthy that several tiny peaks arose in the profile of the  $\text{MnO}_2$ -decorated mesoporous carbon sample upon hydrothermal loading of the Mn species at  $70^\circ\text{C}$ . A comparison with standard PDF cards embedded in MDI Jade (version 6.5) shows that these diffraction peaks are well matched to those of the K-birnessite (JCPDS #80-1098,  $\delta\text{-MnO}_2$ ), implying that  $\text{MnO}_2$  has been successfully decorated over the mesoporous carbon spheres. XPS analyses of both K-NMCS and MK-NMCS samples further confirm that  $\text{MnO}_2$  was completely anchored over the NMCS surface, as evidenced by the Mn 2s, 2p peaks (Figure 1c). Furthermore, the Mn 2p peak was found to show a spin–orbit splitting value of  $11.5\text{ eV}$  (Figure 1d), suggesting that Mn exists in an oxidation state of  $\text{Mn}^{4+}$  in MK-NMCS,<sup>27</sup> in good agreement with the above XRD results.

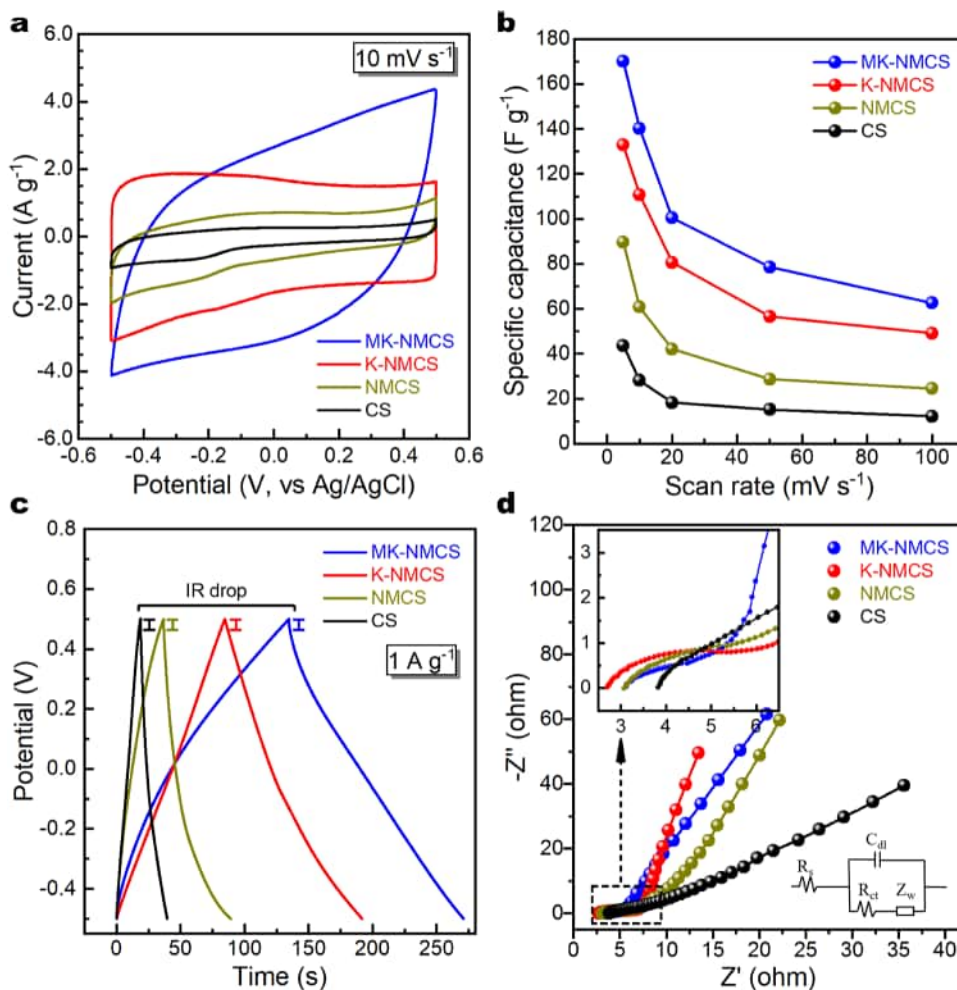
To examine the surface hydrophilicity of the synthetic samples, we measured the water contact angle ( $\theta$ ) evolution of all of these samples at 0 and 30 s, respectively (Figure 1e). Note that the surface of CS obtained from direct pyrolysis is hydrophobic as indicated by the  $\theta$  of  $144.2$  and  $130.1^\circ$  at 0 and 30 s after contact with water. However, after nitrogen doping, the initial  $\theta$  was  $104.6^\circ$  and then decreased to  $75.4^\circ$  after 30 s. It is well-known that nitrogen doping can create various N-containing functional groups, e.g., amines ( $-\text{NH}_2$ ), imides ( $-\text{NH}-$ ), or pyridinic nitrogen ( $-\text{C}=\text{N}-$ ), depending on the doping conditions and the virgin carbon material.<sup>47</sup> Some groups are hydrophilic (such as amines), and others may not be as strongly hydrophilic. A possible explanation for the change in  $\theta$  of the NMCS is that the hydrophilic sites (i.e.,  $-\text{NH}_2$ ) are dominant in the NMCS, which is likely covered by the other hydrophobic groups. The slightly hydrophobic surface of NMCS has been turned into hydrophilic after activation by KOH ( $\theta = 26.2$  and  $2.1^\circ$  at 0 and 30 s); this is attributed to the abundant surface hydroxyl groups anchored by alkaline activation.<sup>21</sup> Interestingly, after decorating  $\text{MnO}_2$  to the K-NMCS, its hydrophilicity has been decreased a little bit, which is believed to be the replacement of surface hydroxyls (with high hydrophilicity) by  $[\text{MnO}_6]$  octahedra (with less hydrophilicity than hydroxyls).

The morphological characters of all of these as-prepared samples are depicted in Figure 2. All of the synthetic materials are monodispersed nanospheres with an average particle size of  $\sim 550\text{ nm}$  (Figure 2a–d). The surface morphologies of CS and NMCS are similar (Figure 2a,b), implying that N-doping appears not to have much effect on the surface morphology. However, the following HF-etching process will undoubtedly



**Figure 2.** SEM images of as-prepared (a) CS, (b) NMCS, (c) K-NMCS, (d) MK-NMCS, and (e) MK-NMCS of higher magnification and (f) the corresponding energy dispersive X-ray (EDX) elemental mapping (note: the elemental compositions in the blue frame area are shown in Figure S2).

create massive surface porosity and roughness in the carbon spheres (Figure 2c).<sup>48</sup> Notably, the SEM image of a higher magnification reveals that the surface of K-NMCS is enriched with hierarchical porosity as KOH activation can remove some carbon atoms to introduce abundant defects,<sup>49</sup> thereby significantly increasing its specific surface area.<sup>41</sup> Upon decorating with  $\text{MnO}_2$ , the resulting MK-NMCS demonstrates a similar surface as K-NMCS, but with less roughness (Figure 2e,f) due to partial filling of the surface pores by  $\text{MnO}_2$  particulates. EDX analysis indicates that the elemental compositions of MK-NMCS are C, N, O, K, and Mn (Figure S2), all of which are uniformly dispersed over the surface of K-NMCS materials (Figures 2f and S2). Besides, the atomic percentage of Mn is  $9.68\%$  (Figure S2), further confirming the XRD and XPS data. The results of the porosity analysis are illustrated in Figure S3. The Brunauer–Emmett–Teller (BET) surface areas of CS, NMCS, K-NMCS, and MK-NMCS are  $299$ ,  $686$ ,  $1267$ , and  $212\text{ m}^2\text{ g}^{-1}$ , respectively (Figure S3a), in good agreement with the SEM images. Note that direct pyrolysis yielded CS with an average pore size of  $7.8\text{ nm}$  (Figure S3b), but copolymerization with TEOS coupled with  $\text{SiO}_2$  removal can expand the pore size to  $11\text{ nm}$  and increase the BET surface area significantly. Interestingly, KOH activation appears to further increase both the BET surface area and the pore, which was also observed elsewhere.<sup>21</sup> Upon decorating with  $\text{MnO}_2$ , the BET surface area decreased expectedly, but only the mesopores of  $15\text{ nm}$  disappeared due to the anchoring of  $\text{MnO}_2$  nanoparticles (Figure S3b), indicating that these  $\text{MnO}_2$  nanoparticles have a particle size in the range of  $5\text{--}15\text{ nm}$ , which is favorable for the diffusion and thereof the intercalation of sodium and heavy metal ions due to the much shorter diffusion pathways of nanosized  $\text{MnO}_2$  compared to bulk  $\text{MnO}_2$ .

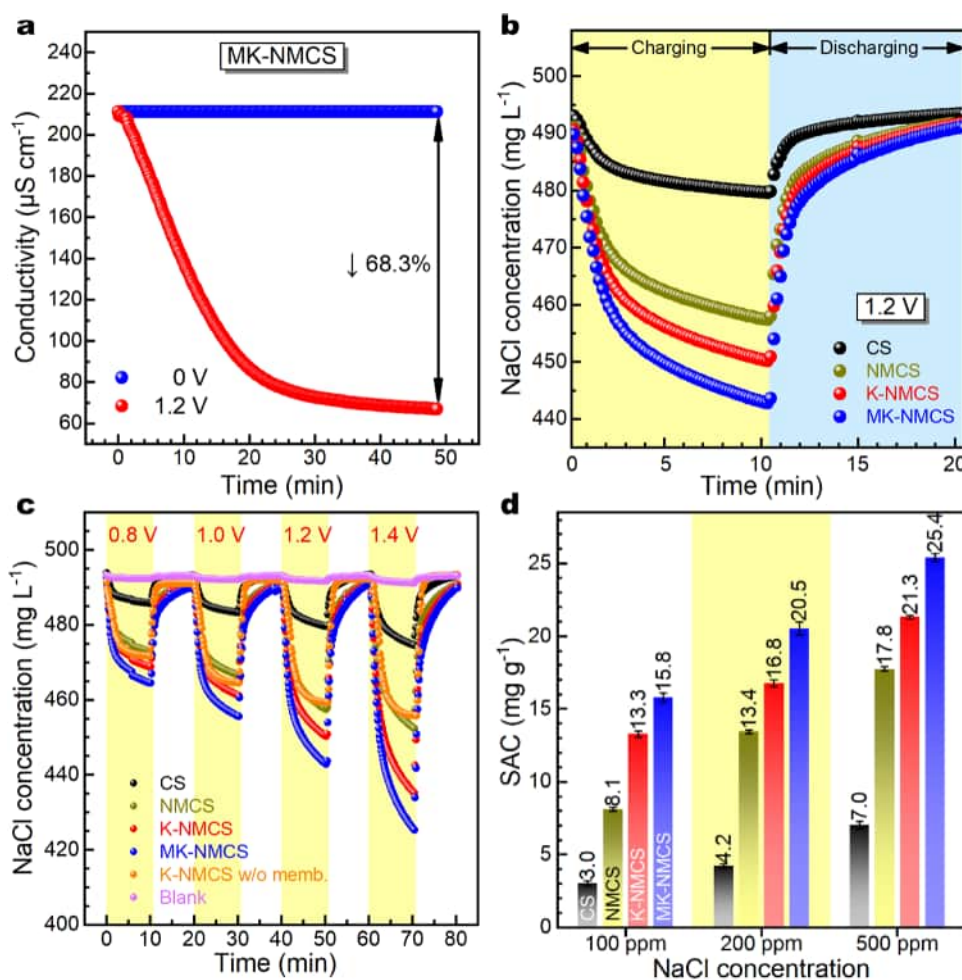


**Figure 3.** Electrochemical characterizations of all mesoporous carbon nanocomposite electrodes: (a) CV curves at 10 mV s<sup>-1</sup> in 1.0 M NaCl solution; (b) specific capacitances at different specific currents; (c) GCD curves at 1 A g<sup>-1</sup> in 1.0 M NaCl solution; (d) Nyquist plots of EIS and the fitting curves, inset in the bottom right corner is the corresponding equivalent circuit.

**3.2. Electrochemical Properties of Electrodes.** As shown in Figure 3a, the CV profiles of all of these mesoporous carbon composite electrodes except MK-NMCS obtained in 1.0 M NaCl solution at 10 mV s<sup>-1</sup> are featured by near-rectangular shapes, indicative of near-ideal capacitive behavior of common carbon-based electrodes.<sup>50</sup> MK-NMCS, in contrast, demonstrated a leaflike-shaped voltammogram, implying a typical less-than-ideal capacitive behavior of redox-active electrodes.<sup>27,51</sup> Specifically, the CV curve is distorted over the potential window of -0.4 to 0.4 V due to the Faradaic reactions ( $\text{MnO}_2 + \text{Na}^+ + \text{e}^- \rightleftharpoons \text{MnOONa}$ ) occurring inside the anchored MnO<sub>2</sub>.<sup>38,51–54</sup> Moreover, the integrated areas under these CV profiles appear to decrease in the order MK-NMCS > K-NMCS > NMCS > CS, indicating the MK-NMCS electrode shows the largest specific capacitance, and probably the best desalination performance (Table S1). The specific capacitances of these electrodes (calculated using eq S1) are negatively correlated with the specific current as expected (Figure 3b) and decrease clearly in the order MK-NMCS > K-NMCS > NMCS > CS. For instance, the MK-NMCS electrode demonstrated a specific capacitance of 170.1 F g<sup>-1</sup> at 5 mV s<sup>-1</sup>, whereas K-NMCS displayed a specific capacitance of 132.9 F g<sup>-1</sup> (versus those of NMCS and CS electrodes, 89.7 and 43.7 F g<sup>-1</sup> obtained at 5 mV s<sup>-1</sup>, respectively). Note that the MK-NMCS electrode with the

smallest specific surface area (212 m<sup>2</sup> g<sup>-1</sup>) shows the highest specific capacitance among all of the electrodes. This is because there is a more important contribution from the Faraday reaction in the MnO<sub>2</sub> particles in addition to the capacitive contribution of the carbon components in the MK-NMCS electrode.<sup>39,55,56</sup>

The GCD curves at 1 A g<sup>-1</sup> in 1.0 M NaCl solution are of nearly symmetric triangles over one cycle of charge–discharge operation, indicating a well-defined and highly reversible character of the capacitive and/or Faradaic behavior during the GCD operation.<sup>27,34</sup> Note that there are *iR* (current resistance) drops at the beginning of each discharge curve but they are too small to be negotiable (Figure S4). The EIS profiles shown in Figure 3d indicate that the charge-transfer resistances (*R*<sub>ct</sub>) of these electrodes are 16.5, 7.3, 3.8, and 4.2 Ω for CS, NMCS, K-NMCS, and MK-NMCS, respectively. This observation confirms that both the nitrogen doping and the KOH activating can greatly reduce the resistance against charge transfer within the carbon materials, thereby boosting the charge migration inside the N-dope carbon electrodes.<sup>21,57</sup> Notably, the *R*<sub>ct</sub> of the MK-NMCS electrode is slightly greater than that of the K-NMCS electrode, which is probably due to partial blocking of the mesopores by the anchored MnO<sub>2</sub> with poor electron conductivity. Furthermore, the steep portion in the intermediate and low-frequency regions (also known as the

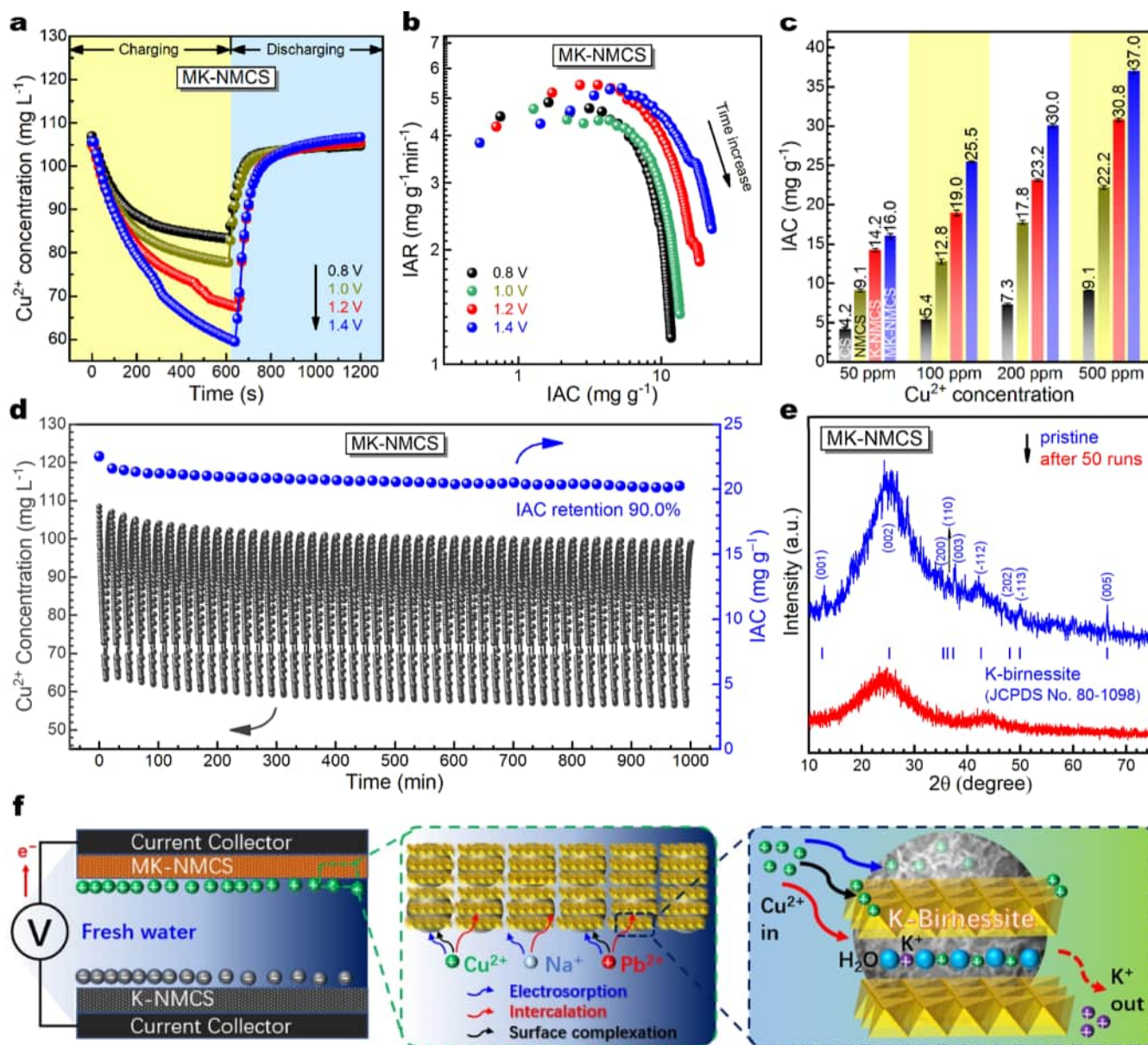


**Figure 4.** (a) Plot of conductivity versus time in the third CDI operation with MK-NMCS electrodes in  $100 \text{ mg L}^{-1}$  ( $1.71 \text{ mM}$ ) of NaCl solution at 0 and 1.2 V, respectively; (b) plots of NaCl concentration during one cycle of charging–discharging operation in CDI cells with different nanocomposite electrodes in  $500 \text{ mg L}^{-1}$  of NaCl solution at 1.2 V; (c) plot of NaCl concentration during the charging–discharging operations in  $500 \text{ mg L}^{-1}$  of NaCl solution at varying voltages (note: “Blank” refers to the graphite paper//graphite paper system, “K-NMCS w/o memb.” denotes the K-NMCS//K-NMCS system without (w/o) ion-exchange membranes; both systems are used as reference); (d) comparison of the SACs of mesoporous carbon nanocomposite electrodes applied to feedwaters with varying NaCl concentrations and at a voltage of 1.2 V.

Warburg impedance,  $Z_w$ ) reflects the frequency-dependent nature of ion transport between the electrolyte and the electrode during the charge–discharge operation. An increase in the slope of the profile indicates a higher level of Warburg impedance. Note that the slopes in the range  $10\text{--}25 \Omega$  decrease in the order  $\text{K-NMCS} > \text{NMCS} > \text{MK-NMCS} > \text{CS}$  (Figure 3d), which implies that the CS electrode has the highest interfacial ion migration rate among these electrodes. Interestingly, the MK-NMCS electrode demonstrates a bit higher  $Z_w$  as compared to that of the CS. A possible explanation is that the partial blocking of mesopores by  $\text{MnO}_2$  hinders the ion migration from the electrolyte to the electrode, as well, thus resulting in a slight increase in the corresponding Warburg impedance.

**3.3. Performance of Capacitive Deionization.** The CDI performance of these electrodes was evaluated in batch mode on an hybrid capacitive deionization (HCDI) platform with various cathode//anode pairs (Table S1). The pairings were designed based on the unique properties of each electrode (Figure 3) and the importance of prefunctionalization of carbon-based electrodes in HCDI.<sup>58</sup> Initially, we chose the MK-NMCS//K-NMCS pair to study the static adsorption of

$\text{Na}^+$  and  $\text{Cl}^-$  onto the cathodes and the anodes in  $100 \text{ mg L}^{-1}$  of NaCl solution. It was found that the conductivity remained the same for  $\sim 50$  min when no cell potential was applied to the HCDI cell (0 V, Figure 4a), implying no static adsorption took place between the electrodes and the electrolyte. This observation is consistent with other previous reports and is believed to be attributed to the barrier effect of ion-exchange membranes (IEMs).<sup>27,38</sup> When a cell potential of 1.2 V was applied, the conductivity of the feed solution decreased dramatically by 68.3% (equivalent to an SAC of  $15.8 \text{ mg g}^{-1}$ ), indicating the capture of both  $\text{Na}^+$  and  $\text{Cl}^-$  by the electrodes. We further examined the CDI performance of these electrode pairs during one full charge–discharge cycle at 1.2 V in  $500 \text{ mg L}^{-1}$  of NaCl solution (Figure 4b). Note that the MK-NMCS electrode exhibited greater salt capture than the other electrodes over the same time interval during the charge operation; in other words, the MK-NMCS electrode demonstrated the greatest salt adsorption rate (SAR), followed by K-NMCS, NMCS, and CS. Calculation with eq 1 reveals that the MK-NMCS electrode has the greatest SAC of  $25.4 \text{ mg g}^{-1}$ , overpassing those of other electrodes (Table S1). This is attributed to the synergistic effect between the cathode and the



**Figure 5.** (a) Plots of  $\text{Cu}^{2+}$  concentration during one cycle of charging–discharging operation in CDI cells with MK-NMCS electrodes in  $100 \text{ mg L}^{-1}$  of  $\text{Cu}^{2+}$  solution at varying voltages; (b) Kim-Yoon plots of the MK-NMCS electrodes in  $100 \text{ mg L}^{-1}$  of  $\text{Cu}^{2+}$  solution at varying voltages; (c) comparison of IAC of all mesoporous carbon nanocomposite electrodes applied to feedwaters with varying  $\text{Cu}^{2+}$  concentrations and at a voltage of 1.2 V; (d) cycling stability and the corresponding IAC of the MK-NMCS//K-NMCS electrode system in  $100 \text{ mg L}^{-1}$  of  $\text{Cu}^{2+}$  solution at 1.2 V; (e) XRD patterns of the MK-NMCS electrodes before and after 50 runs of CDI operation; (f) proposed mechanism of  $\text{Cu}^{2+}$  electroadsorption and intercalation by MK-NMCS electrodes at CDI platforms.

anode, where the Faradaic reactions within  $\text{MnO}_2$  contribute additional  $\text{Na}^+$  ion storage beyond simple capacitive behavior, and the electrical and structural properties of carbon improved by N-doping and KOH activation boost its capturing capacity toward  $\text{Cl}^-$ , allowing for much higher ion capturing capacity.<sup>32,34,56,59,60</sup> Notably, a comparison of these desalination performances indicates that the SAC of the CS//CS pair at 1.2 V was increased by 146.3% after N-doping (Table S1), validating the important contribution of N-doping to the improvement of CDI performance of carbon electrodes.<sup>57,61–63</sup> Likewise, the positive effects of KOH activation and  $\text{MnO}_2$  decoration on the desalination performance were demonstrated by the corresponding SAC increments of 23.4 and 24.5%, respectively. During the discharge operation, the

regeneration rate of these electrodes also follows the same order MK-NMCS > K-NMCS > NMCS > CS, confirming the excellent reversibility of the electrodes once again (Figure 3c) and implying that applying a reverse voltage is an efficient approach to regenerate the electrodes when there are IEMs within the HCDI cell.

To explore the effects of cell voltage and feed concentration on the SAC of these electrodes, we performed the CDI experiments in  $500 \text{ mg L}^{-1}$  of NaCl solution at varying cell voltages (0.8–1.4 V) (Figure 4c) and in feed saline with increasing NaCl concentrations (100–500  $\text{mg L}^{-1}$ ) at 1.2 V (Figure 4d), respectively. It was observed that the NaCl concentration dropped much more rapidly with increasing cell voltage, showing a near-linear increase in SAC for all electrodes

studied (Table S1), which is as expected and consistent with earlier observations.<sup>33,38,45</sup> Note that SACs of the K-NMCS electrode demonstrate a much higher value than those of the K-NMCS electrode without a membrane, verifying the contribution to the SAC from IEMs. For instance, the SAC of the K-NMCS electrode at 1.2 V was increased by 30.8% in the presence of membranes as compared to the counterpart w/o membranes (Table S1). Considering that a cell voltage of 1.4 V usually leads to side reactions such as water splitting (above 1.23 V) and shortening the life span of electrodes,<sup>21,54</sup> like most groups in the CDI community, we chose 1.2 V as the optimal cell voltage. Besides, the salt gradient between the bulk electrolytes and the surface of electrodes is no-double higher in feedwater with higher NaCl concentration, which, in turn, yields a much greater driving force that facilitates the transfer of ions from the bulk electrolytes to the electrodes, thus attaining a higher SAC consequently (Figure 4d). This phenomenon is in good agreement with previous studies.<sup>32,34,57,64</sup> Moreover, the SACs of MK-NMCS electrodes have demonstrated a high SAC comparable to those of other top MnO<sub>2</sub>/C-based electrodes reported in the literature so far (Table S2 and Figure S5).

Given the superior performance of the MK-NMCS electrode, synthetic wastewaters containing either Cu<sup>2+</sup> or Pb<sup>2+</sup> ions (50–500 mg L<sup>-1</sup>) were then used to verify its potential for capacitive removal of both HMs at CDI platforms. As shown in Figure 5a, in 100 mg L<sup>-1</sup> of Cu<sup>2+</sup> solution, the MK-NMCS electrode also demonstrated the same dependence of ion adsorption capacity (IAC, calculated by eq S2) on cell voltage over the range of 0.8–1.4 V as that in NaCl solution (Figure 4b) during one charge–discharge operation. This trend appears once again in the case of 100 mg L<sup>-1</sup> of a Pb<sup>2+</sup> solution (Figure S6a). Further analyses based on the Kim-Yoon plot (Figures 5b and S6b) indicate that applying a higher cell voltage can improve the driving force for ion transfer from the bulk electrolytes to the surface of electrodes, thereby increasing both the IAC and the ion adsorption rate (IAR, calculate by eqs S3 and S4) at a certain time.<sup>13,44</sup> Likewise, the impacts of the Cu<sup>2+</sup>/Pb<sup>2+</sup> ion concentration on the IAC were explored over these electrodes at 1.2 V in solutions with varying Cu<sup>2+</sup>/Pb<sup>2+</sup> concentrations. Irrespective of the type and concentration of both metals, these electrodes show the same trend based on their IACs toward both ions, decreasing in the order MK-NMCS > K-NMCS > NMCS > CS (Figures 5c and S6c). Note that the IAC of the CS//CS for Cu<sup>2+</sup> in 100 mg L<sup>-1</sup> of Cu<sup>2+</sup> solution was increased by 137% after N-doping (Figure 5c), while a further IAC increment of 48.4% was achieved upon KOH activation (K-NMCS versus NMCS). Similar improvements in ion electrosorption capacity were also observed for the CS, NMCS, and K-NMCS electrode pairs in the case of Pb<sup>2+</sup> ions (Figure S6c), due to the structural, chemical, and electrical advantages from N-doping and KOH activation (e.g., larger specific surface area, better wettability, better charge transfer ability, and improved specific capacitance).<sup>21,42,45,57</sup> Their IACs also exhibit the same dependence on metal ion concentration in the bulk electrolytes as observed in the case of the NaCl solution. For instance, the IAC of MK-NMCS toward Cu<sup>2+</sup> is 16.0 mg g<sup>-1</sup> at 1.2 V in 50 mg L<sup>-1</sup> of Cu<sup>2+</sup> solution, whereas it is increased by 59.4, 87.5, and 31.3% in 100, 200, and 500 mg L<sup>-1</sup> of Cu<sup>2+</sup> solutions to 25.5, 30.0, and 37.0 mg g<sup>-1</sup>, respectively (Figure 5c). In addition, the MK-NMCS electrode demonstrates excellent IACs toward both Cu<sup>2+</sup> and Pb<sup>2+</sup> ions (e.g., 30.0 and 37.0 mg g<sup>-1</sup> for Cu<sup>2+</sup>, 32.2

mg g<sup>-1</sup> for Pb<sup>2+</sup> at 1.2 V) under environmentally relevant conditions, which ranks the top of electrodes applied in CDI for capturing both ions,<sup>11,12,15</sup> showcasing its potential for application in heavy metal remediation.

**3.4. Recycling Performance and Potential Mechanism.** Following the same protocol described elsewhere,<sup>38</sup> we chose K-NMCS and MK-NMCS electrodes to conduct the recycling tests. As illustrated in Figures S7 and S8, the cycling stability of the K-NMCS electrode in 500 mg L<sup>-1</sup> of NaCl solution at 1.2 V degrades gradually over time regardless of the presence of IEMs, with a slightly faster rate of degeneration in the absence of IEMs (cf. Figures S7 and S8). For instance, the SAC retention of K-NMCS electrodes w/o a membrane is about 95.4% after 15 consecutive cycles of charge and discharge, while it remains up to 100% in the presence of IEMs under the same conditions (yellow-shaded region in Figure S8). This observation further verifies that the IEMs not only improve the salt uptake but also enhance the short-term cycling stability of the electrodes applied in CDI.<sup>21,22,54</sup> As far as long-term cycling stability is concerned, the structural integrity of the electrodes appears to play a more critical role. Although the K-NMCS electrodes show a SAC retention of 100% over the initial 15 cycles in the presence of IEMs, it continues to decline over time to 82.5% after 50 cycles due to the recession of carbon-based electrodes.<sup>27</sup>

In contrast, the MK-NMCS//K-NMCS electrode system shows excellent cycling stability in 500 mg L<sup>-1</sup> of NaCl solution at 1.2 V, yielding a SAC retention as high as 102.4% after 50 consecutive cycles (Figure S9). Such an abnormal SAC retention (beyond the theoretical value of 100%) is likely to be ascribed to the fact that some of the Na<sup>+</sup> ions are trapped within the MnO<sub>2</sub> lattice during the cycling operations, leading to an apparent SAC that exceeds 100%.<sup>65,66</sup> This is essentially attributed to the intrinsic stability of the electrodes (e.g., the MK-NMCS), the IEMs, and the synergistic effect between the cathode and the anode.<sup>55,67,68</sup> The results of cycling stability tests in 100 ppm of Cu<sup>2+</sup> and Pb<sup>2+</sup> solutions are depicted in Figures 5d and S6d, respectively. The MK-NMCS electrodes also exhibit excellent cycling stability and high SAC retentions. After 50 consecutive cycles, the SAC retentions for Cu<sup>2+</sup> and Pb<sup>2+</sup> were as high as 90 and 98.5%, respectively. The SAC retention of the MK-NMCS electrode for Cu<sup>2+</sup> is slightly lower than that for Pb<sup>2+</sup> ions under the same conditions, even though the hydrated ionic radii of both ions are similar.<sup>69</sup> One possible explanation is that the affinity of MnO<sub>2</sub> for Pb<sup>2+</sup> ions is stronger than that for Cu<sup>2+</sup> ions.<sup>40,70</sup> During the charge–discharge process, both ions undergo capacitive adsorption (electrosorption) within carbonaceous components, insertion inside MnO<sub>2</sub> components, and complexation at the external surface of the [MnO<sub>6</sub>] octahedral layers. The stronger complexation between Pb<sup>2+</sup> and the external surface of the [MnO<sub>6</sub>] layers may help stabilize the layer configuration. Therefore, the repeated charge–discharge process is likely to impair the structural integrity of the MnO<sub>2</sub> component, which likely induces the collapse (deconstruction) of the MnO<sub>2</sub> crystals in the case of Cu<sup>2+</sup> with weaker affinity, ultimately leading to a decrease in SAC retention. Our previous report has also shown that gradual phase degradation of Mn oxides occurs over time upon Cu<sup>2+</sup> ions intercalation/deintercalation.<sup>38</sup> The XRD patterns of the MK-NMCS electrode before and after 50 charge–discharge cycles revealed that the intensity of the MnO<sub>2</sub> diffraction peaks decreased significantly (Figure 5e). This is in good agreement with our earlier

observation,<sup>38</sup> further validating the above speculation of the collapse of MnO<sub>2</sub> crystals after the cycling test.

As mentioned earlier, the N-doped carbon component and the MnO<sub>2</sub> component in the MK-NMCS electrode capture ions by different mechanisms, respectively. Specifically, the N-doped carbon traps Cu<sup>2+</sup> and Pb<sup>2+</sup> ions by electrosorption, while MnO<sub>2</sub> achieves ion capturing by a Faraday intercalation reaction ( $\text{MnO}_2 + 0.5 \text{M}^{2+} + \text{e}^- \rightarrow \text{M}_{0.5}\text{MnO}_2$ ,  $\text{M}^{2+} = \text{Cu}^{2+}$  or  $\text{Pb}^{2+}$ ). Note that Cu<sup>2+</sup> is likely to be reduced to elemental copper upon CDI operations due to its higher standard reduction potential (0.1 V versus saturated calomel electrode (SCE)).<sup>37</sup> But our previous study has excluded this electroreduction reaction of Cu<sup>2+</sup>.<sup>38</sup> Additionally, considering the higher affinity of MnO<sub>2</sub> toward both heavy metals in aqueous solutions, surface complexation reactions between both ions and the external surface of MnO<sub>2</sub> (i.e., [MnO<sub>6</sub>] layer) will undoubtedly take place.<sup>65,70</sup> Collectively, the possible capture mechanisms of Cu<sup>2+</sup> and Pb<sup>2+</sup> ions at the MK-NMCS electrode are likely regulated by three processes: (i) electrosorption (capacitive behavior) within the N-doped carbon component; (ii) insertion inside the [MnO<sub>6</sub>] octahedral interlayers (Faradaic reaction); and (iii) surface complexation at the external surface of the [MnO<sub>6</sub>] layers (Figure 5f). Although it has been well demonstrated that both Cu<sup>2+</sup> and Pb<sup>2+</sup> ions are inserted into MnO<sub>2</sub> via the Faraday reaction;<sup>38,40</sup> however, due to the degradation of the MnO<sub>2</sub> structure after consecutive cycling in the present study (Figure 5e), it is still challenging to uncover the intercalation and deintercalation of both ions into MnO<sub>2</sub> through microstructural characterization. However, the microscopic evidence in favor of the above ion capture mechanisms can be found in MnO<sub>2</sub>/C,<sup>37,38</sup> W<sub>18</sub>O<sub>19</sub>/C<sup>16</sup>, and MoO<sub>2</sub>/C electrodes.<sup>45</sup>

## 4. CONCLUSIONS

A group of MnO<sub>2</sub>-decorated mesoporous carbon nanocomposites was prepared via a multistep approach and then evaluated as electrodes for capturing Na<sup>+</sup>, Cu<sup>2+</sup>, and Pb<sup>2+</sup> ions from wastewaters on an HCDI platform. Benefiting from the intrinsic property of the electrodes, the IEMs, and the synergistic effect between the cathode and the anode, the electrode pair of MK-NMCS//K-NMCS demonstrates the best desalination performance among the electrodes studied, yielding SAC maximums of 33.2 mg g<sup>-1</sup> (1.4 V) and 25.4 mg g<sup>-1</sup> (1.2 V) in 500 mg L<sup>-1</sup> of NaCl solution, respectively. Additionally, the MK-NMCS electrode also shows superior capacities toward Cu<sup>2+</sup> and Pb<sup>2+</sup> ions, offering an IAC as high as 30.0 and 32.2 mg g<sup>-1</sup> in 200 mg L<sup>-1</sup> of Cu<sup>2+</sup> or Pb<sup>2+</sup>-containing note solutions at 1.2 V, respectively. The cycling results reveal that the presence of IEMs can improve the short-term cycling stability and that the MK-NMCS electrode demonstrates excellent cycling stability for all metal ions, attaining SAC retentions of 102.4, 90, and 98.5% over 50 consecutive charge–discharge cycles for Na<sup>+</sup>, Cu<sup>2+</sup>, and Pb<sup>2+</sup> ions, respectively. Mechanism analysis suggests that capacitive electrosorption (by the mesoporous carbon sphere), intercalation (within the MnO<sub>2</sub>), and surface complexation (over the MnO<sub>2</sub> layer, particularly in the case of Cu<sup>2+</sup> ions) are probably responsible for the sequestration of Cu<sup>2+</sup> and Pb<sup>2+</sup> ions. Overall, our findings underscore the potential of the HCDI platform with the MnO<sub>2</sub>-decorated mesoporous carbon sphere, particularly the MK-NMCS//K-NMCS electrodes as an efficient toolbox for the remediation of wastewater contaminated by either Cu<sup>2+</sup> and Pb<sup>2+</sup> ions. Future studies

on the preference of MK-NMCS//K-NMCS electrodes toward specific ions are necessary for fully exploring their potential for ion separation and the recovery of crucial elements from waste streams.

## ■ ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acsami.4c18755>.

Supporting texts (S1–S3), tables (S1 and S2), and figures (S1–S9): CDI setup, N<sub>2</sub> absorption–desorption isotherms, pore size distributions, EDX spectrum, electrochemical characterizations, and CDI deionization performance (PDF)

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### Notes

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